

LISTING OF CLAIMS

This listing of the claims will replace all prior versions and listings of the claims in this application.

Claim 1 (previously presented): A process for preparing mono- or diesters of polytetrahydrofuran or of tetrahydrofuran copolymers comprising polymerizing tetrahydrofuran in the presence of at least one telogen and/or of a comonomer over an acidic catalyst, wherein the polymerization reactor is started up using a mixture of the polymer to be prepared by the process, polytetrahydrofuran, the mono- or diesters of polytetrahydrofuran and/or of the tetrahydrofuran copolymers, tetrahydrofuran, any comonomer and at least one carboxylic anhydride.

Claim 2 (previously presented): The process according to claim 1, wherein the mono- or diesters of polytetrahydrofuran or of the tetrahydrofuran copolymers or the polytetrahydrofuran used for startup have an average molecular weight M_n of from 650 to 4000.

Claim 3 (previously presented): The process according to claim 1, wherein the concentration of the polymer used for startup is from 20 to 80% by weight, based on the total amount of the mixture used for startup.

Claim 4 (previously presented): The process according to claim 1, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.

Claim 5 (previously presented): The process according to claim 1, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

Claim 6 (previously presented): The process according to claim 1, wherein acetic anhydride is used.

Claim 7 (previously presented): The process according to claim 1, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.

Claim 8 (previously presented): The process according to claim 1, wherein an inert solvent is added to the mixture used for starting up the polymerization reactor.

Claim 9 (previously presented): The process according to claim 2, wherein the concentration of the polymer used for startup is from 20 to 80% by weight, based on the total amount of the mixture used for startup.

Claim 10 (previously presented): The process according to claim 2, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.

Claim 11 (previously presented): The process according to claim 3, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.

Claim 12 (previously presented): The process according to claim 2, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

Claim 13 (previously presented): The process according to claim 3, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

Claim 14 (previously presented): The process according to claim 4, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture

used for startup.

Claim 15 (previously presented): The process according to claim 2, wherein acetic anhydride is used.

Claim 16 (previously presented): The process according to claim 3, wherein acetic anhydride is used.

Claim 17 (previously presented): The process according to claim 4, wherein acetic anhydride is used.

Claim 18 (previously presented): The process according to claim 5, wherein acetic anhydride is used.

Claim 19 (previously presented): The process according to claim 2, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.

Claim 20 (previously presented): The process according to claim 3, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.